

A NEW RHEOMETRICAL EQUIPEMENT FOR THE CHARACTERIZATION OF LARGE GRANULAR MATERIALS INVOLVED IN FAST LANDSLIDES

Anna Maria Pellegrino¹, Anna Scotto di Santolo², Aldo Evangelista³ and Leonardo Schippa¹

¹Department of Engineering, University of Ferrara, Italy; ²Pegaso University, Italy; ³University of Napoli Federico II, Italy.

ABSTRACT

The present study focused on novel rheometrical tool for the determination of the rheological behaviour of large particle mixtures with particular interest in the application to granular materials involving in fast landslides as mud and debris flows. The main goal is the development of the Sphere Drag Rheometer (SDR), a home-made large-scale rheometer that allow to estimate the rheological properties of these mixtures considering the whole grain size distribution. The SDR is composed of a sphere rigidly joined to a support that moves at constant velocity into the mixture. Compared to standard rheometer, the SDR uses much higher volume of mixtures of wider grain size distribution next to that in situ. Several pyroclastic soils collected from the source area of debris flows occurred in Campania region (Southern Italy) were analyzed. The paper reports the experimental results on fine particles mixtures, large particle mixtures, and their comparison.

Keywords: Four or Five Keywords (First Characters of Each Word are in Capital/Uppercase Letters), Italic

INTRODUCTION

The paper focuses on an innovative rheometrical system for the determination of the rheological properties of fluids containing large particles, i.e. maximum grain size larger than 1 mm. The knowledge about the rheological properties of large particle fluids is of great and increasing importance because of their relevance in several fields like natural hazards, building materials, gas and oil, and food industry [1]. In the present study fast landslides as debris flows and the application of rheometry for debris flows are of primary interest. Debris flows put in danger people and animals, and cause damage in hilly and mountainous areas. More than 55000 people died in the last hundred years worldwide due to debris flows or combined debris flow and flood events. In Italy more than 4000 people die from 1963 to 2012 due to debris flows and flooding phenomena. In order to protect people, animals and infrastructures from damage, hazard zone mapping and warning systems as well as structural protective measures must be considered depending on the specific situation. During the definition process of such protective measures, the debris flow modeling is a fundamental task [2]-[3]. Numerical and physical modeling help in the hazard zones delineating and in the structural design and testing [4]. In order to understand and simulate the flow and the deposition process, an appropriate rheological model is a very useful physical concept for mud, debris and hyper-concentrated flows [5]. The simplest method is to assimilate the flowing mass to

a continuous viscous fluid and refers to rheological models derived from the resistance formula of Newtonian and Non-Newtonian fluids [6]. When a rheological model is considered, only the material flow curve, e.g. expressing the shear rate-shear stress relation, is required. Nowadays, efficient rheometrical apparatuses for the determination of the rheological parameters of mixtures and fluids containing fine particles exist and the experimental methods related to them are widely consolidated [5]-[7]-[8]-[9]-[10]. For mixtures and fluid containing large particle, the study of the influence of the grain size is more complicated. Experimental devises equipped with a large geometrical configurations are required and such apparatuses are few and not commercially developed [11]-[12]-[13]-[14]-[15]. The debris flow materials hereby considered presents a wide grain size distribution and a small content of fine particles. Therefore, in order to estimate the rheological properties of these mixtures (i.e., considering the whole grain size distribution), a home-made experimental large-scale rheometer was design and built, the Sphere Drag Rheometer (SDR). The system could be an efficient rheometrical tool for the investigation of fluids containing particles up to 10 mm grain size.

THE SHERE DRAG RHEOMETER SDR

Characteristics and procedures

Referring to the works of [14]-[16], we developed an innovative system for measuring the motion's resistance for large particle mixtures called

SDR. The SDR is composed of a sphere, with variable diameters D , rigidly joined to a support that moves at constant velocity into the mixture. The sphere is connect to a load cell that measures the drag force necessary to move the ball through the fluid at the imposed speed. The system, illustrated in Fig. 1, is composed by a cylindrical container (i.e. having radius d_c equal to 130 mm, height h_c equal to 60 mm and sample volume equal to 0.5 l) in which the material sample are located and of an eccentric sphere (i.e. with a variable eccentricity r , relative to the motor, varying from 20 to 46 mm) fixed to a thin vertical shaft. Differently from conventional apparatus, the SDR rheometer allows to consider larger sample volume (0.5 l in SDR versus 30 ml in standard rheometers) and larger grain size distribution (up to 10 mm grain size in SDR versus 0.5 mm grain size in standard rheometer). The device can be equipped with different spheres having diameters ranging from 8 to 18 mm. The main components of the SDR apparatus are (see Fig. 1): a base station with two motors (i.e., a “slow motor” goes from 0.4 to 9.5 rpm and a “fast motor” goes to 10 to 260 rpm); a telemeter as broadcasting system; load cells having different full scale FS (i.e., one equal to 250 g and the other equal to 1000 g); a box for the electronica controlling; a reed (i.e. a magnetic position sensor); a software called SMV_V1 developed ad hoc for the SDR rheometer control.

The experiment consists in measuring the drag force F_D at a specified rotational speed Ω , while the sphere makes one full rotation within the material sample.

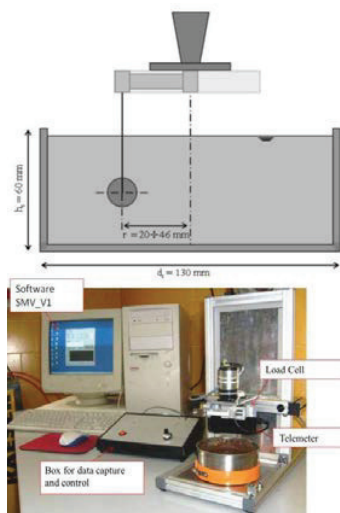


Fig. 1 Upside: geometrical scheme of the SDR rheometer. Downside: complete configuration of the SDR rheometer.

In Fig. 2a the measured points, obtained during one full rotation of the sphere, for different values of

Ω , are showed. For each imposed velocity the value of the required drag force F_D (value at which the sphere starts moving through the material sample) is evaluated as the average between the measured points in a full rotation, of the sphere, as illustrated in Fig. 2b. The apparent flow curve was obtained by applying an increasing and decreasing rotational speed ramp. In order to ensure the stability of the measurements, each value of velocity was imposed for 30 seconds. This time was in agreement with the experimental results carried out with conventional rheometer on the same pyroclastic debris flow materials as described in [5].

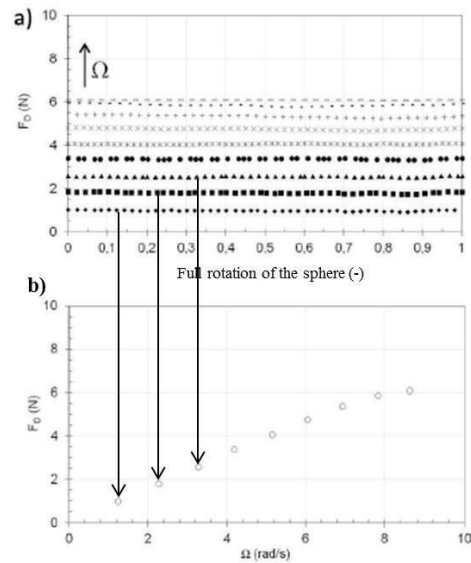


Fig. 2 Silicon oil with viscosity equal to 60 Pa·s. a) Measurements of F_D during a full rotation of the sphere ($D = 18$ mm) at different values of the imposed rotational speed Ω (diamonds 1.24 rad/s, squares 2.27 rad/s, triangles 3.28 rad/s, circles 4.19 rad/s, stars 5.15 rad/s, crosses 6.93 rad/s, little dashes 7.83 rad/s, big dashes 8.63 rad/s); b) Resulting flow curve F_D - Ω .

Calibration of the SDR rheometer

The SDR rheometer was calibrated using several reference materials for which the rheological behaviour was already analyzed and well-known. Tests were performed on different Newtonian viscous materials (i.e. glycerin and silicone oils at different peculiar viscosity) and on Non-Newtonian viscous materials with yield stress (i.e. hair gel and tomato sauce). After, the calibration was carried out using a representative soil-water mixture, composed by water and kaolin, in order to approach the feasibility of the experimental apparatus with particles-fluid suspensions close to debris flow material mixtures tested in traditional rheometer

before [5]. The kaolin-water mixture was reconstituted according to the total solid volumetric concentration Φ_T , defined as the ratio of the volume of solids to the total volume (water plus solids), as follow:

$$\Phi_T = \frac{V_S}{V_{TOT}} = \frac{V_S}{V_S + V_W} = \Phi_f + \Phi_g \quad (1)$$

where V_{TOT} , V_W , V_S are, respectively, the total volume, the volume of water and the volume of solid in the sample, and Φ_f , Φ_g are, respectively the solid volumetric concentration of fine particle and the solid volumetric concentration of coarse particle of the mixture. The complete description of the calibration is reported in [17].

Conversion of measured data into rheological parameters

Unlike traditional rheometers, the measuring system adopted for the SDR is not based on the classic shear flow between two parallel surfaces but on the flow regime around the object, a sphere that moving as in Fig. 3. For this reason it was defined an appropriate theory of conversion that allow to relate the two schemes of flow.

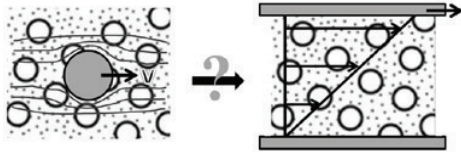


Fig. 3 Schematic principal task for the sphere drag measuring system on the left. Scheme of the classic shear flow on the right.

The analytical solution of the free motion of an object into a Newtonian fluid goes back to the work of [18]-[19] reported in [20]. The problem of the motion of an object of spherical shape through a Yield Stress Fluid is more complex than the case of Newtonian Fluid and requires a different treatment. No simple solutions were found yet and various analytical expressions were also been proposed [21]-[22]-[23]. All the theoretical works, which assume a simple yielding behavior, predict a particle velocity progressively decreasing to zero as the applied force tends to the critical value for incipient motion. The experimental results presented in the literature are in agreement with this basic expectation, namely, that the object can move through the fluid only when the force applied to it becomes greater than a critical one. In the case of Yield Stress Fluid we assume that the fluid remains perfectly rigid in its solid regime and follows a constitutive equation such as Herschel & Bulkley in its liquid regime as:

$$\tau = \tau_c + k \cdot \dot{\gamma}^n \Rightarrow \tau > \tau_c \quad (2)$$

In equation (2), τ is the shear stress (Pa), τ_c is the yield stress (Pa), $\dot{\gamma}$ is the shear rate (s^{-1}), k is the consistent coefficient ($Pa \cdot s^n$) and n is the dimensionless pseudo-plasticity index. The considered conversion theory is applicable only in the treatment of Yield Stress Fluid. As observed in [5] the soil-mixtures considered in the present study are Yield stress Fluid and their behaviour is well described using the Herschel & Bulkley model (equation (2)). In this condition the drag force F_D can be computed as following:

$$\frac{F_D}{F_C} = 1 + \frac{k}{\tau_c} \cdot \dot{\gamma}_{app}^n \quad (3)$$

Where k is an increasing, positive, dimensionless function of the surface of the object and decrease towards a critical, minimum value k_c and F_C is the critical drag force F_C equal to:

$$F_C = 4\pi \cdot R \cdot \tau_c \cdot k_c \quad (4)$$

Where R is the sphere radius. Considering the numerical work of [23], the relationship between the measured sphere velocity and the apparent shear rate is the following:

$$\dot{\gamma}_{app} = \frac{v}{l} \quad (5)$$

Where v is the linear velocity of the sphere (m/s) and l is equal to 1.35 multiplied the radius of the sphere R . The complete description of the applied conversion theory is reported in [17].

MATERIALS AND METHODS

The SDR experimental results reported are related to pyroclastic soils which are representative of real pyroclastic debris flows occurred in Southern Italy. The soil mixture analyzed with SDR were before tested with standard rheometer as reported in [5]. The soil A and B derives from the most recent deposits produced by the volcanic activity of mount Somma/Vesuvius and they are sandy silt with a small clay fraction. The geotechnical and mechanical properties of such materials are well documented in literature [24]. All the experiments involved mixtures of dry soils with different amounts of water. The materials were mixed with appropriate amount of distilled water in order to obtained mixtures having different solid volumetric concentrations Φ according to equation (1). The range of solid concentration here considered was defined according to natural porosity of the soils and taking into consideration the previous study of [5]. A total amount of about 500 ml of mixture (distilled water and soils) was pre-pared and each sample was continuously mixed for the time needed to obtain a fairly homogeneous mixture. The whole sample was used performing SDR test. The entire experimental program was carried out at constant temperature

equal to 23°. Fine-grained mixtures (i.e., mixtures composed by soil fraction with a particle diameter less than 0.5 mm) were tested in order to compare the data to those obtained using standard rheometer [5]. Also coarse-grained mixtures (i.e., mixtures composed by soil fraction with a particle diameter up to 0.5 mm) were tested. The complete experimental program is illustrated in table 1. A total amount of about 500 ml of mixture (distilled water and soils) was pre-pared and each sample was continuously mixed for the time needed to obtain a fairly homogeneous mixture. The whole sample was used performing SDR test. The entire experimental program was carried out at constant temperature equal to 23°.

Table 1 Experimental program.

Test (#)	Soil (-)	Φ_T (%)	Φ_f (%)	Φ_g (%)	d_{MAX} (mm)
1	A	35	35	-	0.5
2	A	38	38	-	0.5
3	A	40	40	-	0.5
4	A	42	42	-	0.5
5	A	35	28	7	5.0
6	A	38	31	7	5.0
7	A	40	32	8	5.0
8	A	35	21	14	10.0
9	A	38	24	16	10.0
10	B	32	32	-	0.5
11	B	35	35	-	0.5
12	B	38	38	-	0.5
13	B	30	21	9	5.0
14	B	32	22	10	5.0
15	B	35	25	10	5.0
16	B	38	29	9	5.0

RESULTS AND DISCUSSION

The fine-grained water-soil A and B mixtures were tested with SDR rheometer according to experimental program described in Table 1. The experimental data obtained are reported in Figures 4 and 5 for soil A and soil B, respectively, at different solid volumetric concentrations Φ . The graphs report the evolution of the drag force F_D as a function of the apparent shear rate. For each mixtures considered, the apparent shear rate was derived from the value of the imposed rotational speed Ω according to equation (5). In this way we defined the experimental flow curve in which the measured drag force F_D is related to the calculated apparent shear rate. Then the experimental flow curves (e.g., symbols in Figures 4 and 5) were compared with the theoretical curve (e.g., lines in Figures 4 and 5) obtained starting to the conversion theory and using

the equations (3) and (4). First, we note that there is a good match between the measured data and those obtained through the application of the conversion theory. The water-soil mixtures behave like Non-Newtonian fluid and flow resistance increases with the increasing of shear rate regardless the value of solid concentration. The solid fraction clearly influences the rheological behavior of the materials. Although it is not possible to precisely identify the value of the critical drag force F_D associated to each mixtures, especially for more dilute mixtures (e.g., because of the lack of measurement points at very low rotational speed), even though the data show a trend equal to that obtained with tests in standard rheometer [5]. The resistance force is strictly influences by the solid volumetric concentration. The intrinsic strength of the mixtures increases as the particle fraction increases and there is a critical value of drag force below which the flow is possible. The coarse-grained water-soil A and B mixtures were tested with SDR rheometer according to experimental program described in Table 1. The experimental data obtained are reported in Figures 6 and 7 for soil A and soil B, respectively, at different solid volumetric concentrations Φ and different grain size distribution. The graphs report the evolution of the drag force F_D as a function of the apparent shear rate. For each mixtures considered, the apparent shear rate was derived from the value of the imposed rotational speed Ω according to equation (5). In this way we defined the experimental flow curve in which the measured drag force F_D is related to the calculated apparent shear rate. Also in this case, the coarse-grained water-soil mixtures behave like Non-Newtonian fluid and the flow resistance increases with imposed shear rate regardless the value of solid concentration.

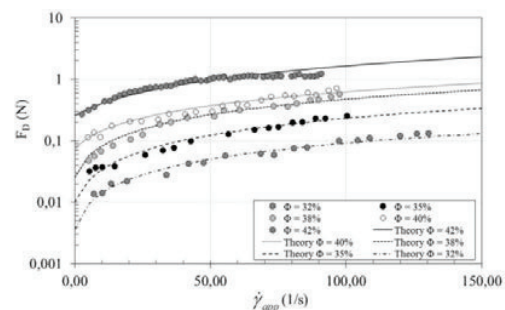


Fig. 4 Fine-grained water-soil A mixtures at several values solid volumetric concentration Φ : comparison between SDR measured data (symbols) and theoretical curve (lines).

The solid fraction also influences the rheological behavior of the materials. The data show a trend equal to that obtained with tests on fine-grained mixtures.

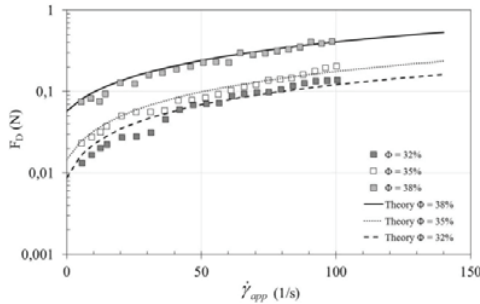


Fig. 5 Fine-grained water-soil A mixtures at several values solid volumetric concentration Φ : comparison between SDR measured data (symbols) and theoretical curve (lines).

We note that the resistance force is strictly influenced by the grain size distribution and increases as the size particles increases (Fig. 6) according to [12] and [13]. The experimental results obtained on coarse-grained water-soil A and B mixtures were compared with those obtained on fine-grained water-soil A and B mixtures according to experimental program described in Table 1. The comparisons obtained are reported in Figures 8 and 9 for soil A and soil B, respectively, at different solid volumetric concentrations Φ and different grain size distribution. We observe that, at equal total solid volumetric concentration, the adding of the solid fraction with a diameter less than 5 mm brings to a reduction of the characteristic resistance of the mixture regardless the material tested. Moreover, when you consider that the addition of the fraction of particles with a diameter less than 5 mm corresponds to a solid volumetric concentration of coarse particles Φ_g of about 8-10% of the entire total solid concentration, this result becomes consistent with several previous experimental observations ([12]-[13]) and with the experimental results obtained through tests on the same coarse-grained mixtures with conventional measurement systems reported in [15]. Several studies have already demonstrated that the addition of coarse particles brings to an increase of the rheological characteristics of the mixture but, for relatively low solid volumetric concentration, a minimum depletion in fine particles fraction within the mixture does not seem to be sufficient to induce an increase of rheological parameters ([12]-[13]-[14]- [15]). Different considerations can be done when the solid fraction with a diameter less than 10 mm is added. We observe that, at equal total solid volumetric concentration, there is an increase of the characteristic resistance of the mixture. Indeed, it is noted that the addition of the fraction of particles with a diameter less than 10 mm corresponds to a solid volumetric concentration of coarse particles Φ_g of about 14-16% of the entire total solid concentration.

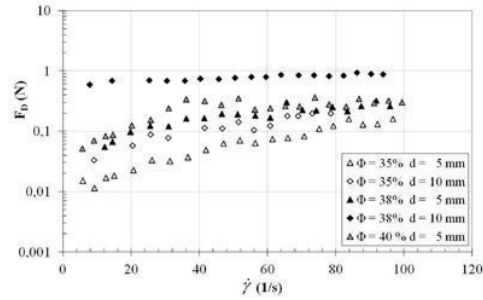


Fig. 6 Coarse-grained water-soil A mixtures at several solid volumetric concentration and grain size distribution according to Tab. 1.

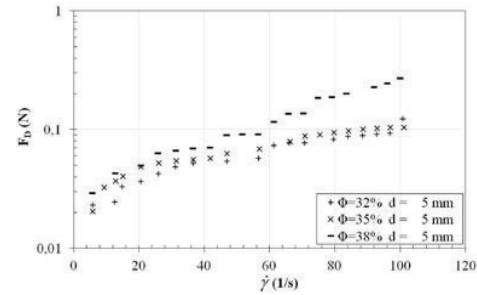


Fig. 7 Coarse-grained water-soil B mixtures at several values solid volumetric concentration Φ and grain size distribution according to Tab. 1.

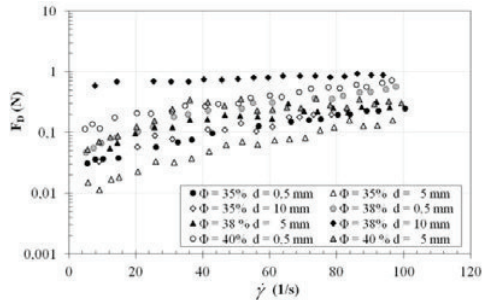


Fig. 8 Water-soil A mixtures: comparison between fine-grained and coarse-grained mixtures according to Tab. 1.

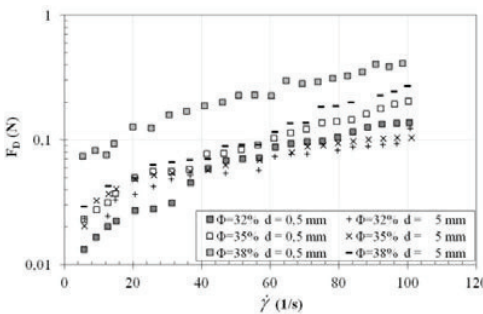


Fig. 9 Water-soil B mixtures: comparison between fine-grained and coarse-grained mixtures according to Tab. 1.

CONCLUSIONS

The obtained experimental results, conveniently converted into rheological parameters, show that the SDR rheometer is able to analyze flowing materials similar to those involved into pyroclastic debris flow.

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